



A six-compound, high performance gasoline surrogate for internal combustion engines: Experimental and numerical study of autoignition using high-pressure shock tubes

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A six-compound, high performance gasoline surrogate for internal combustion engines: Experimental and numerical study of autoignition using high-pressure shock tubes

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Abstract

This paper presents experimental and modeling data for the autoignition of a novel, six-component, high performance gasoline surrogate fuel comprising ethanol, *n*-heptane, *i*-octane, 1-hexene, methylcyclohexane, and toluene (AL-P-I-O-N-A). Experimental tests are conducted in two high-pressure shock tubes to determine the ignition delay time as a function of pressure, temperature and equivalence ratio. Ignition delay times were measured at 10 and 30 bar in the temperature range from 749 to 1204 K and equivalence ratios ranging from 0.35 to 1.30. A modified Arrhenius equation is defined to mathematically describe the ignition delay time of the proposed surrogate. For experimental data with temperatures higher than 900 K, a multiple linear regression identified the pressure dependence exponent of 0.72 and stoichiometry dependence exponent of 0.62, as well as a global activation energy of ≈ 109 kJ/mol. A simplistic approach to mechanism reduction based on the elimination of reactions with no relevant rate of progress was used in order to reduce an extensive detailed kinetics model (hierarchically constructed with more than 17800 reactions). The reduced detailed kinetics model with 4885 elementary reactions among 326 chemical species was used for numerical simulations. Comparisons between the experimental and numerical data are favorable, with the predictions using the reduced kinetics model differing by less than 0.056% when compared to the complete mechanism. It was observed that for low temperatures the proposed reduced kinetics model agrees only qualitatively with the measurements. In order to understand the likely cause of this discrepancy a brute force sensitivity analysis on IDT was performed, elucidating the more influencing reactions on the ignition delay times. The experimental data obtained in this research was compared to available data in the literature in terms of anti-knock index (AKI) and for a scaled pressure of 30 bar (τ_{30}) at a stoichiometric composition. A modified Arrhenius equation was then fitted and an AKI dependence exponent of -1.11 was obtained, inferring that the higher the AKI the higher the IDT, independent of fuel composition at temperatures lower than the NTC region. This trend should be confirmed by further studies.

Keywords: Multicomponent gasoline surrogate, High-pressure shock tube, Reduced chemical kinetics mechanism, Brute force sensitivity analysis.

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1. Introduction

Vehicle propulsion technologies employing internal combustion engines (ICE) are being pushed to a higher level of performance, mainly because of future emissions regulations. The European Commission (EC) has adopted a new regulatory proposal establishing that the average emissions of the EU fleet of new cars must drop by 15% in 2025 and by 30% in 2030, compared to their respective limits in 2021 [1]. In order to comply with these regulations and satisfy well-to-wheel sustainability requirements, the research in internal combustion engines has focused in a host of strategies in new combustion concepts, control and after-treatment systems [2]. The combustion solutions for light and medium vehicles include the use of alternative fuels, such as biofuels [3], compressed natural gas (CNG) [4], and liquid petroleum gas (LPG) [2], and advanced combustion strategies, such as homogeneous charge compression ignition (HCCI) [5, 6, 7, 8, 9, 10, 11], reactivity-controlled compression-ignition (RCCI) [12], and lean combustion, high-compression ratio, spark controlled, gasoline compression ignition (GCI) [13].

HCCI engines provide a higher thermal efficiency compared to spark ignition (SI) and compression ignition (CI) engines, producing lower levels of nitrogen oxides (NO_x) and particulate matter (PM), as well as near-zero soot emissions [14, 15]. One of the major challenges in HCCI is to control the timing of the auto-ignition event, which is responsible for initiating the CI combustion process [14, 15, 16]. In SI engines auto-ignition may cause an abnormal combustion known as knocking, which affects the engine's overall performance [17]. A fuel with a higher knocking resistance allow the engine to run at higher efficiency at high loads when knocking is limiting [18, 19]. With such high performance gasoline fuels, the control of compression ratio, valve timing and variable intake system allow to take advantage of the higher fuel knocking resistance [20]. Therefore, the formulation of new high performance gasoline fuels requires to investigate the dependence of ignition delay time on temperature and pressure in order to predict the conditions that lead to the start of combustion in HCCI mode, or the onset of knocking in SI engines.

The ignition delay time (IDT) is defined as the time interval from the elapsed time when the air/fuel mixture reaches a pressure and temperature condition sufficient to ignite it to when the mixture actually auto-ignites [21, 22]. Mathematical correlations can be used to predict the IDT of a practical fuel. These equations are based on traditional Arrhenius expressions and may have from three to dozens of parameters [23, 24]. For different kinds of fuels, in addition to temperature and pressure, some researchers have proposed equations involving the use of other parameters such as oxygen percentage [24], octane number (ON) [25], equivalence ratio [26], carbon chain length [27], among others. In this study, the ignition delay time correlation is expressed according to a modified Arrhenius expression [28, 29] as

$$\tau_{\text{ing}} = A \times \exp\left(\frac{E_a}{RT}\right) \times p^{-x} \times \phi^{-y}, \quad (1)$$

where A is the pre-exponential factor, E_a is the global apparent activation energy, R is the universal gas constant, x and y are the pressure and stoichiometry dependence coefficients respectively. Eq. 1 is advantageous because its input values are parameters directly measured on the test facilities, and because it is known to provide a good curve-fit of IDT measurements especially at high temperatures ($T > 1000$ K) [21, 29].

A single Arrhenius correlation is not able to describe a two-stage ignition since it does not capture the cool flame phenomenon [30, 31], which is exhibited by paraffin class fuels and varies significantly with the hydrocarbon structure. Normal paraffins, such as n -heptane and n -decane, give strong cool flames, while branched chain paraffins are more resistant to ignition [30]. The cool flame phenomenon is usually associated with negative temperature coefficient (NTC) behavior, in which the reaction rate decreases with increasing temperature in the intermediate temperature region ($650 \text{ K} < T < 1000 \text{ K}$) [32].

The ignition delay time of a fuel mixture can be determined in different types of test facilities, such as high-pressure shock tubes (HPST) and rapid compression machines (RCM) [33]. Studies of practical gasoline fuels are quite scarce [34] given that it is very difficult to investigate them in any great detail, as these fuels comprise approximately one hundred different chemical species, making any detailed combustion modeling / characterization process very difficult to achieve [35]. Chemical surrogates allow to approximate the thermal ignition of the real fuels. Many researchers have conducted IDT measurements for the development and validation of global and detailed chemical kinetics models for fuel surrogates with great success [35, 36] and this is the strategy adopted here.

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80 Additionally, there are few studies with high performance (AKI > 90) gasolines, with most data obtained from engine tests [37, 38, 39]. Agbro *et al.* [40] employed a rapid compression machine to obtain IDTs of a gasoline/*n*-butanol blend and a TRF (RON = 95) surrogate for $\phi = 1.0$ at₁₄₀
85 20 bar and 678–858 K. Results showed that the effect of *n*-butanol as an octane enhancer were above what should be expected based on a simple linear blending law. Sarathy *et al.* [41] performed extensive testing of two FACE (Fuels for Advanced Combustion Engines) gasolines, FACE F and FACE G, using both an RCM and a shock tube,₁₄₅
90 for $\phi = 0.5$ and 1.0, at 20 and 40 atm at temperatures from 650 to 1270 K. Results at temperatures above 900 K were similar for both fuels but intermediate temperature data showed stronger NTC behavior for the FACE F gasoline, which had a lower octane sensitivity. Simulations per₁₅₀
95 formed with various proposed surrogates demonstrated a significant kinetic coupling between cycloalkanes and aromatics, affecting the radical pool population.

In this work, a novel, six-compound gasoline surrogate with anti-knock index of 95.5 (AKI = (RON + MON)/2),₁₅₅
100 is developed to emulate a high-performance gasoline. This surrogate has 27 % vol. ethanol in the composition, thus being representative of a potential Brazilian high performance gasoline with a relatively high oxygenated biofuel content [42]. The ignition delay time for this surrogate is,₁₆₀
105 measured in two different high-pressure shock tube facilities, a reduced chemical kinetics mechanism is developed and the important reactions are elucidated using sensitivity analysis. The results may be used for engine combustion development and also as a baseline for future fuel,₁₆₅
110 optimization.

1.1. Gasoline surrogates

Practical gasoline contains different kinds of substances distributed mainly among linear and branched straight-₁₇₀
115 chain alkanes, cyclo-alkanes, aromatics, and olefins [43]. Gasoline surrogates are formulated to represent a practical gasoline while simultaneously maintaining its chemical and physical characteristics, such as ignition delay time, burning velocity, viscosity, density, vaporization, octane,₁₇₅
120 rating, and emissions [35, 44, 45], as well as spray behavior (spray break-up, penetration and dispersion angle) [46, 47].

In the formulation process of a surrogate, a reliable approach to ensure the prediction of numerous combustion₁₈₀
125 targets of the real fuel is to include one or more components from each hydrocarbon class in the surrogate, ensuring that at least one molecular structure of each class is represented [44].

A single component gasoline surrogate such as *iso*-₁₈₅
130 octane is able to reproduce flame propagation characteristics [48], however it would be inconsistent to choose this single compound to represent a practical fuel with a research octane number (RON) higher than 100. On the other hand, a five-component gasoline surrogate might be
135 able to predict simultaneously a practical fuels RON value

in addition to its ignition delay time [35, 49, 42]. Thus, in recent years there has been a growing interest in the formulation of ternary mixtures (*n*-heptane/*iso*-octane/toluene) and other multi-component mixtures, spanning the carbon number range from C₄ to C₁₀ [50].

1.2. Chemical groups used for gasoline surrogates

A multi-component gasoline surrogate is usually formed by mixing four or more species comprising the most common hydrocarbon compounds in a practical fuel. In the literature the compounds frequently used are: linear paraffin (*n*-pentane or *n*-heptane), branched paraffin (*iso*-pentane or *iso*-octane), aromatic (toluene), naphthene (cyclopentane, cyclohexane or methylcyclohexane) and olefin (1-hexene, 1-pentene or *di-iso*-butylene) [36, 45, 49, 42, 51, 52, 53, 54]. Oxygenate surrogates additionally include an oxygenated compound (ethanol, butanol, MTBE, ETBE, etc.) [42, 50, 55].

Alcohols (AL), especially ethanol, are added to practical gasoline mainly to reduce both dependence on fossil fuels and pollutants emission [56]. Ethanol addition leads to a significant reduction in hydrocarbon (HC) and NO_x emissions [57]. Moreover, as ethanol has a high knock resistance, it can increase the overall octane rating of the ethanol-containing gasoline [42, 58].

In a practical gasoline the *n*-paraffinic (P) content is usually in the range from 7 to 14 mol.%, while *iso*-paraffins (I) are found in the range from 29 to 45 mol.% [45]. Paraffins, particularly *n*-paraffins, have a unique low-temperature chemistry that can lead to knock in SI engines and may facilitate ignition in HCCI engines [59]. The knocking tendency of *n*-paraffins increases with the length of the carbon chain, while *iso*-paraffins present a decreased knock tendency because of the side chains, especially when the methyl groups (CH₃) are found in the second from the end or center position of the basic carbon chain [30].

Olefins (O) are hydrocarbon compounds with one or more carbon double bonds and are normally present in gasoline in small quantities, around 3 to 7 mol.% [45]. One double bond has little antiknock effect, while the presence of two or three bonds considerably increases the antiknock effect [30]. Because of their chemical structure, olefins can increase the reactivity of a gasoline as well as improve the gasoline octane number [60, 61]. Naphthenes (N) are saturated hydrocarbons that contain one or more rings, each of which may have one or more paraffin side chains [62].

Aromatics (A) are similar to naphthenes, but they contain a resonantly-stabilized unsaturated ring core [63]. Naphthenes are present in gasoline generally in the range from 1 to 20 mol.%, while aromatics are found in concentrations up to 35 mol.% [45]. Aromatics have a greater knock resistance than their corresponding sized naphthenes. In both groups of fuels the presence of two or more double bonds appreciably increases a fuels resistance to knock [30].

1.3. The GSBR1 (AL-P-I-O-N-A) gasoline surrogate

The present study proposes a novel, six-compound gasoline surrogate (dubbed GSBR1) to emulate a high performance gasoline. This surrogate has a measured anti-knock index of 95.5 [RON = 101.5, MON = 89.5] (Bontorin, A.C.B; Rouge, A; Oliveira, E.J. CENPES / PETROBRAS²³⁵ - Personal communication, 2019). Additionally the GSBR1 has 27 vol.% ethanol in the composition, modeling a potential Brazilian high performance gasoline [42]. Table 1 shows the compounds as well as the volumetric percentage on mixture. All compounds were acquired from Sigma-²⁴⁰ Aldrich[®].

Table 1: Composition of the gasoline surrogate GSBR1 proposed in this work

| Group | Species | CAS Number | Purity (%) | Concentration (vol.%) |
|-------|-------------------|------------|------------|-----------------------|
| AL | Ethanol | 64-17-5 | ≥99.5 | 27.0 |
| P | <i>n</i> -Heptane | 142-82-5 | ≥99.0 | 11.5 |
| I | <i>i</i> -Octane | 540-84-1 | ≥99.0 | 30.0 |
| O | 1-Hexene | 592-41-6 | ≥99.0 | 5.0 |
| N | MCH | 108-87-2 | ≥99.0 | 7.0 |
| A | Toluene | 108-88-3 | ≥99.9 | 19.5 |

MCH: Methylcyclohexane

AL: Alcohols, P: *n*-Paraffins, I: *i*-Paraffins, O: Olefins

N: Naphthenes, A: Aromatics

2. Experimental approach

Two experimental facilities were used in this work, which are briefly described in the following.

2.1. High-pressure shock tube at IVG/UDE

The experimental facilities and procedures are described⁴⁶⁰ in earlier studies [52, 64, 65, 66, 67]. Gas mixtures were prepared by injecting the liquid gasoline surrogate mixture into an evacuated, heated stainless-steel mixing vessel, with subsequent complete evaporation. The total amount of fuel mixture and the added air were controlled mano-²⁶⁵ metrically in order to ensure the desired equivalence ratio. The mixture was stirred for two hours. All of the experiments were performed with the shock tube, the mixing vessel and all connecting gas lines pre-heated to 50°C. The shock speed was measured over two intervals using three piezo-electric pressure gauges. Pressure data were²⁷⁰ recorded with a time resolution of 0.1 μ s.

All ignition delay times shown in this work were determined by extrapolating the steepest increase of the CH* chemiluminescence emission (at 431 nm) signal to its zero level on the time axis as shown in Figure 1(a). To account for the appearance of a cool flame, a second photomultiplier (PMT) was operated to measure CH₂O chemiluminescence in the 400 to 450 nm wavelength range. The estimated uncertainty in reflected shock temperature is less than ± 25 K. The experiments were carried out using synthetic air containing 79% N₂ and 21% O₂. The driver gas was mixed in-situ by using two high-pressure mass-flow controllers. Helium was used as the main component

and argon was added to match the acoustic impedance of the test gas. Concentrations of 5 to 20% Ar in He were required to generate tailored shock waves.

2.2. High-pressure shock tube at C3/NUIG

The high-pressure shock tube at C3/NUI Galway has been described in detail previously [34, 68, 69, 70] and is only briefly discussed here. This facility consists of a stainless steel tube of 8.76 m in length, with an internal diameter of 6.3 cm. A double-diaphragm section divides the shock tube into a 3 m long driver section and 5.73 m driven section. Aluminum plates were used as diaphragms in all experiments, with thicknesses varying from 1.0-1.4 mm depending on the desired temperature behind the shock wave T_5 . The driver gas used was helium, with the eventual addition of nitrogen to achieve tailored driver gas conditions which allow for longer test times [71].

The diagnostic system consists of two digital oscilloscopes (TiePie Handyscope HS4) and six pressure transducers (PCB model 113A24) which measure the incident shock wave velocity at five locations separated by known distances, with the shock velocity extrapolated to the endwall. This extrapolated velocity was used to calculate the conditions, T_5 and p_5 , behind the reflected shock wave using the CHEMKIN II [72]. The pressure at the endwall was monitored using a pressure transducer (Kistler 603B) and the ignition delay time was defined as the interval between the pressure rise due to the arrival of the incident shock wave at the endwall and the subsequent maximum rate of pressure rise, as shown in Figure 1(b).

2.3. Uncertainties related to the shock-tube experiments

There are several uncertainties associated with ignition delay times measured in shock-tube experiments. The more representative systematic errors are related to the mixture preparation, position of pressure and chemiluminescence devices, formation of boundary layer and optical access of the chemiluminescence sensor to the region of test.

2.3.1. Liquid GSBR1 mixture and reactive mixture preparation

Liquid mixtures of GSBR1 were prepared by volume (see Table 1 for compounds and percentages) and manually blended and stirred in the liquid phase for 30 min. As the surrogate fuel is a liquid at room temperature, the reactive test mixtures were prepared by a direct injection method. The mixing tanks were evacuated to 0.1 mbar and heated to 70°C. Thereafter, the fuel was injected using a gas-tight syringe, and its partial pressure was measured using a pressure transducer and digital readout. After injection of the liquid blend into the mixing vessel, the surrogate begins to evaporate. Around 90 minutes later, the pressure inside the vessel is measured and compared to the value calculated theoretically using Dalton's law, taking into account all of the compounds in the mixture of the

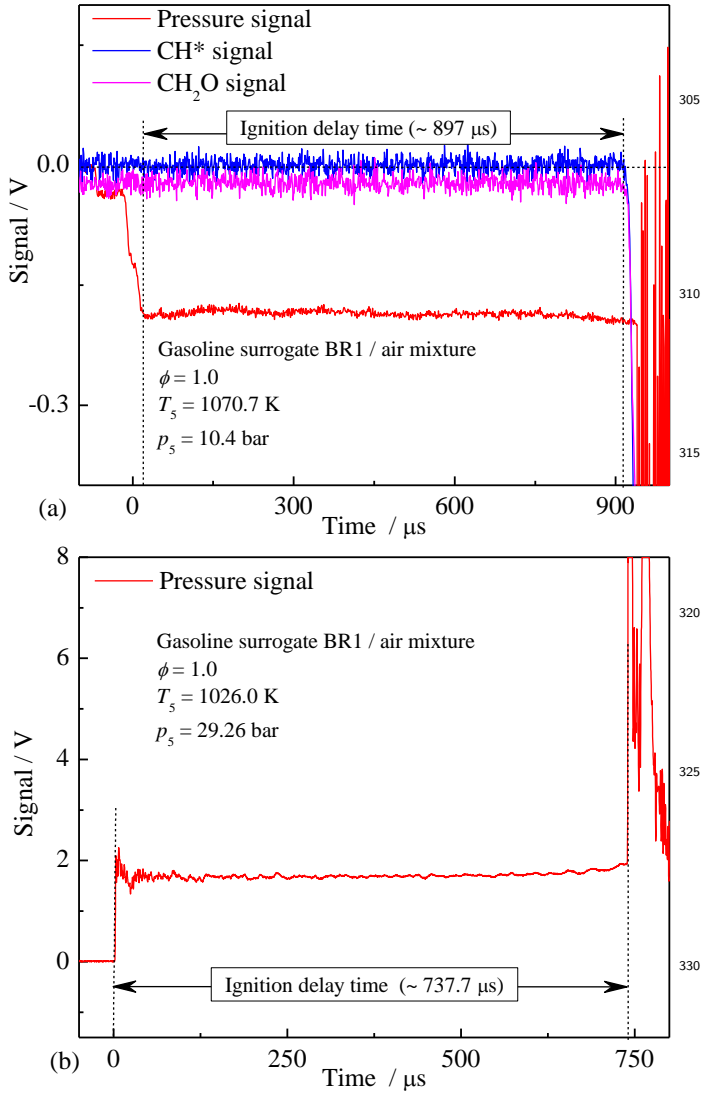


Figure 1: Ignition delay time definition at (a) HPST at IVG/UDE, (b) HPST at C3/NUIG

gasoline surrogates. In this work, there was no difference between the measured and calculated values of pressure after injection of the mixture into the mixing vessels at both IVG/UDE and C3/NUIG. This confirms that there was complete evaporation of the liquid mixture. In addition, the vapor pressure values of the compounds in the mixture must be taken into account. The vapor pressure must be above the required partial pressure of a particular compound. After complete evaporation of the liquid mixture, the vessel is then manometrically filled with synthetic air (21% O₂ and 79% N₂), until the pressure reaches the calculated value of p_{vessel} (for a set of experiments with constant stoichiometry, ϕ).

For each experiment, the test section of the HPST was carefully filled (manometrically) to a target p_1 in order to reach the desired condition of p_5 and T_5 after incident and reflected shock waves [35, 65]. Both mixture vessels are stirred magnetically (at C3/NUIG) or mechanically (at

IVG/UDE), which: (a) ensures the homogenization of the reactive mixture and, (b) helps to reduce the possibility of stratification due to the density difference among the mixture components. The pressure transducers have an accuracy of 0.5% FS (full span), which results in an estimated error of about $\pm 0.9\%$ in the equivalence ratio of the mixture, ϕ .

2.3.2. Shock speeds measurements

In both devices the incident shock wave velocities were determined using piezoelectric pressure transducers close to the endwall of the test section, with shock attenuations of 0.7%/m to 2.5%/m. The measured shock velocities were then compared to the initially estimated values of the incident shock waves, with differences of about $\pm 0.3\%$ being observed. Thereafter, the reflected shock conditions were determined according to standard one-dimensional shock relations. Using the SHOCK module in CHEMKIN II [72], uncertainties of about $\pm 0.3\%$ in the incident wave speed yielded variations in the calculated T_5 of about ± 7 K, and variations in the calculated ignition delay time of about $\pm 7.5\%$. This is in agreement with the experimental uncertainties (temperature and ignition delay time) reported in the literature [35, 73, 74]. In this work, the estimated uncertainties in ignition delay times are in the range of $\pm 7.5\%$ to $\pm 11\%$.

2.3.3. Boundary layer effects in shock tubes

In shock tube experiments there are several non-ideal effects that influence the measurement of ignition delay time. When modeling IDT in shock tubes, perfectly homogeneous reactor conditions (zeroth order approximation model) are used and then, the numerical results are compared to the measurements [35, 65]. The simulation also assumes that behind the shock wave the spatial and temporal conditions are uniform, i.e., the incident and reflected shock waves travel through the test gas and leave it unperturbed. In a real shock-heated gas there is the formation of a boundary layer at the tube wall, that grows with time given the propagation of the shock wave and the movement of the contact surface [35, 65, 75]. Observed effects of boundary layer formation and growth behind the incident shock wave include a gradual increase in temperature and pressure in the core of the flow (T_2 and p_2). When the shock wave returns as a reflected shock, it sets the temperature and pressure (T_5 and p_5) to values higher than those calculated initially using the Rankine-Hugoniot relations. Also, the displacement of the reflected shock wave also creates a boundary layer behind it, affecting the temperature and pressure (T_5 and p_5). Petersen and Hanson [76] proposed a methodology to evaluate this source of systematic error in high-pressure shock tubes, with a relation between the relative change of T_5 with reflected shock test time ($dT_5^*/d\tau_{\text{ing}}$). Equation 2 presents this relative change on temperature T_5 for larger diameter shock tubes

355 (~ 15 cm).

$$\frac{dT^*}{d\tau_{\text{ing}}} \approx 10 \text{ s}^{-1} \quad (2)$$

For shock tube diameters smaller than 10 cm the relative change ($T^* = \Delta T_5 / T_{5\text{-initial}}$) increases to values of 20 s^{-1} to 30 s^{-1} . Assuming that boundary layer effects have a major systematic error on temperature, and for shock tube diameters of 9 cm (IVG/UDE) and 6.3 cm (C3/NUIG). In this work values of 20 s^{-1} and 26 s^{-1} (respectively) were assumed for the determination of uncertainties in both HPSTs. Tables 2 and 4 show the estimated values of ΔT_5 for all of the IDTs measured in this work.

365 2.4. Experimental conditions 405

Experiments were carried out covering a wide range of operation conditions, i.e., temperatures, pressures, and equivalence ratios as found in internal combustion engines (SI and HCCI engines). Table 2 summarizes all of the experimental conditions studied in this work. Information related to the absolute mole fraction of each component for all equivalence ratios can be found as supplementary material.

Table 2: Experimental conditions for IDT measurements in this work 415

| | |
|---|--------------------------|
| Mixture | GSBR1 in synthetic air |
| Pressures, (bar) | 10 - 30 |
| Stoichiometries, ϕ | 0.35 - 0.7 - 1.00 - 1.30 |
| Temperature range, (K) | 749 to 1204 |
| GSBR1 compounds and volumetric percentage (vol.%): | |
| Ethanol/ <i>n</i> -Heptane/ <i>i</i> -Octane/1-Hexene/Methylcyclohexane/Toluene | |
| 27.0/11.5/30.0/5.0/7.0/19.5 (vol.%) | |
| Synthetic air (21% O ₂ and 79% N ₂) | |

3. Numerical approach 425

Numerical simulations of the IDT experiments were conducted using the CANTERA software, version 2.4.0, [77]. Simulations were performed assuming an isochoric - adiabatic homogeneous reactor. Numerically, the thermal ignition was defined as the time of maximum OH concentration along the simulation process [35, 49, 78].

3.1. Reduced chemical kinetics model

In this work, a reduced kinetics model is proposed, based on a detailed mechanism from the CRECK modeling group at Politecnico di Milano (POLIMI TOT 1412 kinetics mechanism, Version 1412, December 2014) [79]. The POLIMI TOT 1412 model was constructed in a hierarchical way by adding to a base core-kinetics model the chemical sub-mechanisms for other species with molecular mass larger than those of the core kinetics. The development and validation of this mechanism employed a vast amount

of experimental data of laminar flame speeds of hydrocarbons and oxygenated fuels including C₀ to C₄ species, reference fuels, alkanes (*n*-heptane, *iso*-octane, *n*-decane, *n*-dodecane), cyclo-alkanes (cyclohexane and methyl-cyclohexane), aromatics (benzene, toluene, xylene and ethylbenzene), oxygenated fuels (C₃H₆O isomers, dimethyl ether and ethyl tertiary butyl ether), and methyl esters up to methyl decanoate [79]. As a result, the POLIMI TOT 1412 mechanism has 17848 elementary reactions among 451 species. The fine agreement observed across the entire range of conditions investigated was used to confirm the reliability and validity of the kinetics model. The mechanism was also validated by comparing predicted and calculated ignition delay time in shock tubes and concentration profiles of the isomers of butanol (*n*-butanol - *n*-C₄H₉OH), *sec*-butanol - *sec*-C₄H₉OH), *iso*-butanol - *iso*-C₄H₉OH, and *tert*-butanol - *tert*-C₄H₉OH) measured in batch reactors, plug-flow reactors and in a jet-stirred reactor [80, 81].

Even though CANTERA can reasonably handle such extensive mechanisms for ignition delay time simulations, it is unwieldy to compute phenomena like laminar flame speed. In order to reduce the detailed mechanism, a script, native to CANTERA, was employed. In summary the script runs an IDT simulation and, at each time step, ranks the elementary reactions according to their relative net reaction rate. In order to obtain an adequate reduced mechanism the simplification procedure was carried out as follows: (1) a set of simulation conditions was used as reference; equivalence ratios $\phi = 0.35, 0.70, 1.00$ and 1.30 , temperatures of $T = 800 \text{ K}$ and 1100 K , and pressures of $p = 10 \text{ bar}$ and 30 bar . This set of conditions results in 16 simulations for each mixture to be compared (full mechanism against reduced mechanism). (2) all IDT cases were computed using a constant volume, adiabatic, homogeneous reactor model using the full mechanism, thus defining a reference IDT to be compared to the IDT obtained from the reduced kinetics model. (3) comparisons were performed testing the predictions of the reduced model for each of the six pure components of the GSBR1 surrogate as well as the complete blend, therefore resulting in 224 simulations (112 each for both the full and reduced mechanisms). (4) a maximum relative difference (Equation 3) of 0.1 (%) was defined in order to set the stop criteria for reaction number reduction. On each case the top 4000 reactions were selected, with the final reduced, yet still quite detailed, mechanism comprising 4885 reactions among 318 chemical species.

$$\text{Rel}_{\text{diff}}(\%) = \left[\frac{\text{IDT}_{\text{full_mech}} - \text{IDT}_{\text{red_mech}}}{\text{IDT}_{\text{full_mech}}} \right] \times 100 \quad (3)$$

Figure 2 shows the relative difference (Equation 3) obtained in all simulations performed along the reduction process. It is important to note that the reduction process was performed by comparing numerical to numerical data, while no experimental validation was performed for mechanism reduction.

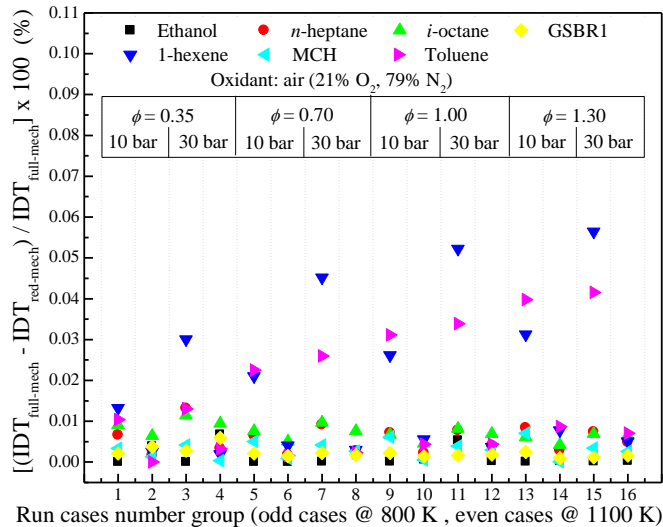


Figure 2: Relative difference of predicted ignition delay times (IDT) using the full model [79] and the reduced model proposed in this work.

It can be observed that the relative difference defined in Equation 3, for all of the mixtures numerically tested was below 0.056% for all conditions of ϕ , T and p investigated. Figure 2 shows that moving in the direction of rich mixtures, the relative difference in IDT predictions increases for toluene and 1-hexene. For the others fuels tested, the relative difference was quite constant and below 0.02%. The threshold of 0.1 (%), defined as stop criteria for reaction number reduction in Equation 3, yields a reduced kinetics model with 4885 elementary reactions among 318 species. Table 3 presents a comparison of both kinetics mechanisms as well as the average time for the simulations. The reduced mechanism (in CANTERA format) as well as the glossary of species are available as Supplementary Material.

Table 3: Main characteristics of the detailed kinetics model [79] and the reduced kinetics model proposed in this work.

| Mechanism | Detailed [79] | Reduced |
|------------------------------|---------------|---------|
| Elements | 5 | 5 |
| Species | 451 | 326 |
| Reactions | 17848 | 4885 |
| Average time per run* | 50 s | 12 s |

* Constant volume homogeneous reactor simulation in CANTERA [77] - Computation performed in a personal computer Intel Core i7-5500U CPU @ 2.40 GHz

4. Results and discussion

4.1. Ignition delay time measurements

The two facilities used covered a wide range of pressure, temperature and stoichiometry in the experiments using the GSR1. Tables 4 and 5 list all the experimental data measured using both HPSTs. Figure 3(a) shows the data trend for experiments at IVG/UDE. Figure 3(b) shows the data trend for the experiments at C3/NUIG.

Figure 3(c) shows the experimental data from both HPSTs. Several observations can be made at this point. The IDT data trends do not show any NTC behavior, indicating that the volumetric percentage of n -paraffins (11.5% n -heptane) does not impact the overall reaction rate at low temperatures ($T < 950$ K). Figure 3(c) shows the good agreement between the data recorded using both facilities, with measurements in the range of $1200 \text{ K} < T < 980 \text{ K}$ overlapping for the pressures and equivalence ratios investigated.

The data can be fitted to an equation of the form of Equation 1 using multiple linear regression analysis with $\ln(\tau_{\text{ing}})$ as the dependent variable and $(1000/T_5)$, $\ln(p)$ and $\ln(\phi)$ as independent variables identified the value of $x = 0.72$ and $y = 0.62$, as well as a global activation energy of $\approx 109 \text{ kJ/mol}$. Equation 4 shows the fitted expression in the modified Arrhenius from.

$$\tau_{\text{ign}}/\mu\text{s} = 10^{(-1.66 \pm 0.18)} \exp\left(\frac{109 \pm 3.40 \text{ kJ/mol}}{RT}\right) (p/\text{bar})^{(-0.72 \pm 0.06)} \phi^{(-0.62 \pm 0.06)} \quad (4)$$

The coefficient of determination of the multiple linear regression was $R^2 \approx 0.95$ for the experimental data shown in Tables 4 and 5, from both the facilities. The fitting was determined for the experimental data using temperatures above 900 K, considering the pressures and stoichiometries from Table 2.

It can be clearly seen that the T -dependence of auto-ignition delay times flatten when moving from the high- to low-temperature regime and that the global activation energy drops for temperatures below 900 K. Similarly, these changes in the τ_{ing} slope are also observed in many experimental results in the literature for different fuels [21, 35, 49, 82, 78, 83, 84].

4.2. Numerical predictions using the reduced kinetics model

Figure 4 shows the numerical prediction of all of the experimental data reported in Tables 4 and 5.

Several observations can be made from this comparison. The first is that the reduced kinetics model reproduced the experimental results comparatively well in the high to middle temperature range investigated in this work ($1200 \text{ K} \lesssim T \lesssim 900 \text{ K}$), and the accuracy increases as equivalence ratio increases. Also, the proposed reduced model reproduces the bend in the experimental data for $p = 30 \text{ bar}$ and $\phi = 1.0$ at low temperatures, while for leaner mixtures and low pressures the reduced model is able to qualitatively follow the experiments.

4.2.1. Brute-force sensitivity analysis on IDT

In order to better understand the reduced ability to predict the ignition delay times at low temperatures, a brute force sensitivity analysis on IDT was performed.

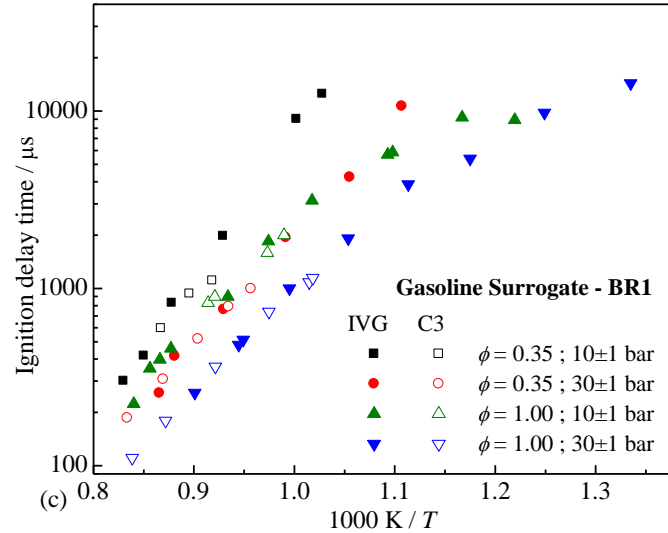
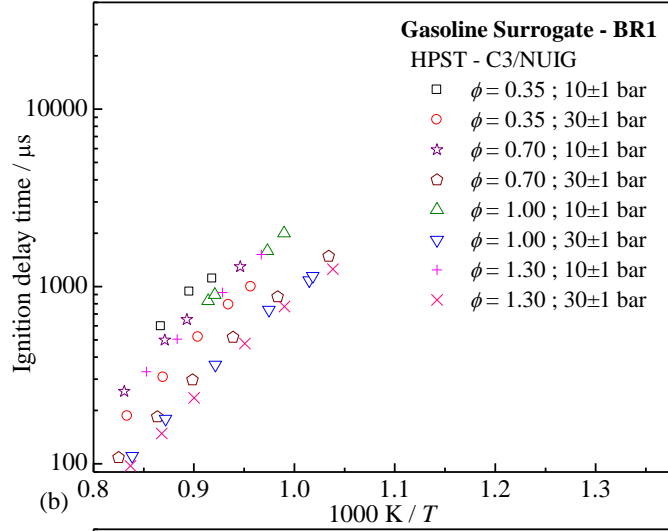
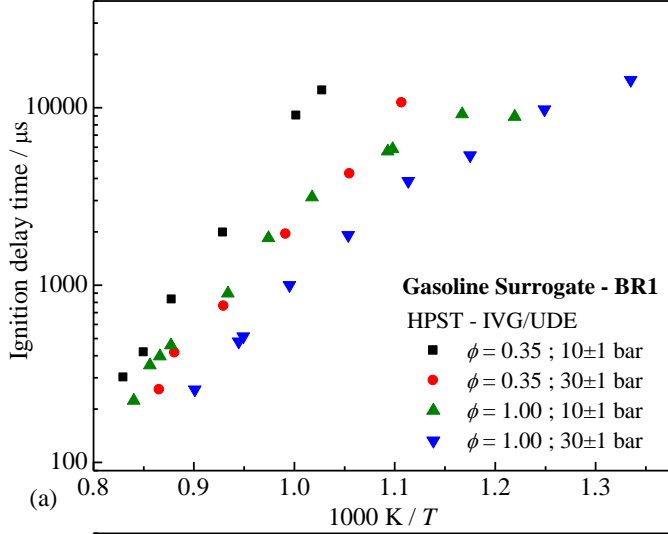


Figure 3: Experimental IDT data from (a) IVG/UDE, (b) C3/NUIG and (c) IVG/UDE and C3/NUIG at the same experimental conditions of pressure and equivalence ratio

Simulations were performed for twenty-four sets of conditions: temperatures of 750 K, 900 K and 1050 K, stoi-

Table 4: Gasoline surrogate BR1 ignition delay time measurements at IVG/UDE

| ϕ | T_5 (K) | $\pm\Delta T_5$ (K) | p_5 (bar) | τ_{ing} (μs) |
|--------|-----------|---------------------|-------------|---------------------------------------|
| 0.35 | 1205.1 | 0.7 | 10.0 | 301.3 |
| 0.35 | 1176.4 | 1.0 | 10.5 | 417.2 |
| 0.35 | 1139.2 | 1.9 | 10.8 | 829.9 |
| 0.35 | 1076.5 | 4.3 | 10.5 | 1975.7 |
| 0.35 | 997.9 | 18.0 | 9.9 | 9028.2 |
| 0.35 | 973.0 | 24.3 | 10.6 | 12495.9 |
| 0.35 | 907.2 | *** | 10.2 | N.I ^a |
| 0.35 | 1155.2 | 0.6 | 30.2 | 257.3 |
| 0.35 | 1135.1 | 0.9 | 32.1 | 415.3 |
| 0.35 | 1075.5 | 1.6 | 31.5 | 759.9 |
| 0.35 | 1008.4 | 3.9 | 30.5 | 1938.2 |
| 0.35 | 947.6 | 8.0 | 29.6 | 4243.1 |
| 0.35 | 903.4 | 19.3 | 30.2 | 10674.4 |
| 0.35 | 831.1 | *** | 33.0 | N.I ^a |
| 0.35 | 750.4 | *** | 30.0 | N.I ^a |
| 1.00 | 1190.3 | 0.5 | 10.7 | 223.6 |
| 1.00 | 1167.8 | 0.8 | 9.3 | 353.7 |
| 1.00 | 1154.4 | 0.9 | 9.1 | 397.1 |
| 1.00 | 1140.2 | 1.0 | 10.8 | 458.0 |
| 1.00 | 1070.7 | 1.9 | 10.4 | 897.0 |
| 1.00 | 1026.6 | 3.8 | 10.6 | 1846.8 |
| 1.00 | 982.6 | 6.2 | 10.8 | 3130.6 |
| 1.00 | 915.0 | 10.4 | 10.4 | 5683.3 |
| 1.00 | 910.8 | 10.7 | 10.2 | 5865.3 |
| 1.00 | 856.9 | 15.8 | 10.2 | 9198.6 |
| 1.00 | 820.0 | 14.6 | 10.6 | 8908.7 |
| 1.00 | 767.9 | *** | 10.6 | N.I ^a |
| 1.00 | 1110.1 | 0.6 | 30.4 | 257.8 |
| 1.00 | 1058.8 | 1.0 | 30.4 | 481.0 |
| 1.00 | 1053.5 | 1.1 | 30.0 | 513.0 |
| 1.00 | 1004.8 | 2.0 | 30.1 | 998.9 |
| 1.00 | 949.1 | 3.6 | 29.7 | 1914.4 |
| 1.00 | 898.2 | 6.9 | 29.7 | 3866.0 |
| 1.00 | 851.1 | 9.2 | 30.0 | 5394.8 |
| 1.00 | 800.6 | 15.6 | 29.9 | 9764.7 |
| 1.00 | 749.1 | 21.5 | 29.8 | 14344.3 |

^aN-I = no ignition within the test time

chiometries were set at $\phi = 0.35$ and $\phi = 1.00$, and two points of pressures were analyzed (10 and 30 bar), with the perturbation being generated by multiplying the reaction rate (k) of each reaction of the reduced model by 0.5 and 2.0, and then calculating the IDT for each perturbation. Each brute force sensitivity analysis, programmed in CANTERA [77] took 47.5 hours running in a HP - Workstation Intel Xeon E5420 CPU @ 2.50 GHz.

Equation 6 shows the sensitivity criteria adopted in this work for the brute force analysis. Therefore, if the sensitivity (S) is zero, the perturbed reaction has no influence on IDT, if the sensitivity (S) is higher than zero, the perturbed reaction increases the IDT (positive influence) and conversely it reduces the IDT (negative influence).

$$S_{(\text{sensitivity})} = \frac{\tau_{\text{with perturbation}}}{\tau_{\text{without perturbation}}} - 1 \quad (5)$$

Table 5: Gasoline surrogate BR1 ignition delay time measurements at C3/NUIG

| ϕ | T_5 (K) | $\pm\Delta T_5$ (K) | p_5 (bar) | τ_{ing} (μs) |
|--------|-----------|---------------------|-------------|---------------------------------------|
| 0.35 | 1152.3 | 1.8 | 9.7 | 596.5 |
| 0.35 | 1116.7 | 2.7 | 9.7 | 935.7 |
| 0.35 | 1089.0 | 3.1 | 9.7 | 1109.0 |
| 0.35 | 1199.4 | 0.6 | 29.7 | 186.0 |
| 0.35 | 1150.0 | 0.9 | 30.1 | 307.3 |
| 0.35 | 1105.8 | 1.5 | 30.4 | 519.0 |
| 0.35 | 1070.0 | 2.2 | 30.7 | 788.7 |
| 0.35 | 1045.0 | 2.7 | 30.8 | 995.3 |
| 0.70 | 1204.0 | 0.8 | 9.6 | 256.4 |
| 0.70 | 1148.0 | 1.5 | 9.9 | 497.7 |
| 0.70 | 1120.0 | 1.9 | 10.3 | 650.5 |
| 0.70 | 1057.0 | 3.6 | 10.0 | 1293.0 |
| 0.70 | 1212.0 | 0.3 | 30.3 | 108.6 |
| 0.70 | 1185.0 | 0.6 | 30.1 | 184.4 |
| 0.70 | 1112.7 | 0.9 | 30.4 | 297.8 |
| 0.70 | 1065.0 | 1.4 | 30.6 | 517.0 |
| 0.70 | 1017.0 | 2.3 | 30.9 | 873.8 |
| 0.70 | 967.0 | 3.7 | 30.9 | 1482.0 |
| 1.00 | 1094.0 | 2.4 | 9.3 | 830.0 |
| 1.00 | 1086.0 | 2.5 | 9.7 | 897.0 |
| 1.00 | 1027.5 | 4.2 | 9.3 | 1589.0 |
| 1.00 | 1010.2 | 5.3 | 9.4 | 2000.0 |
| 1.00 | 1192.5 | 0.3 | 29.1 | 110.6 |
| 1.00 | 1147.0 | 0.5 | 29.8 | 179.2 |
| 1.00 | 1085.5 | 1.0 | 29.7 | 361.4 |
| 1.00 | 1026.0 | 2.0 | 29.3 | 737.7 |
| 1.00 | 985.3 | 2.8 | 29.6 | 1081.0 |
| 1.00 | 981.9 | 2.9 | 30.1 | 1147.0 |
| 1.30 | 1173.0 | 1.0 | 9.4 | 331.0 |
| 1.30 | 1132.0 | 1.5 | 9.5 | 504.7 |
| 1.30 | 1077.0 | 2.6 | 9.4 | 925.5 |
| 1.30 | 1034.0 | 4.1 | 9.5 | 1517.0 |
| 1.30 | 1195.0 | 0.3 | 29.3 | 97.5 |
| 1.30 | 1152.0 | 0.4 | 29.8 | 148.5 |
| 1.30 | 1111.0 | 0.7 | 30.3 | 235.5 |
| 1.30 | 1051.8 | 1.3 | 29.7 | 476.7 |
| 1.30 | 1010.0 | 2.0 | 30.3 | 770.3 |
| 1.30 | 963.0 | 3.1 | 30.7 | 1252.0 |

530 Reactions with sensitivities below the threshold were then ignored for plotting. Figures 5 and 6 shows the classical bars diagram for perturbation of 0.5 and 2.0 respectively.

535 The analysis pointed out the following twenty-two reactions as the most influencing of the reduced kinetics model (4885 reactions), taking the threshold value of 0.5 % change (absolute) on the IDT:

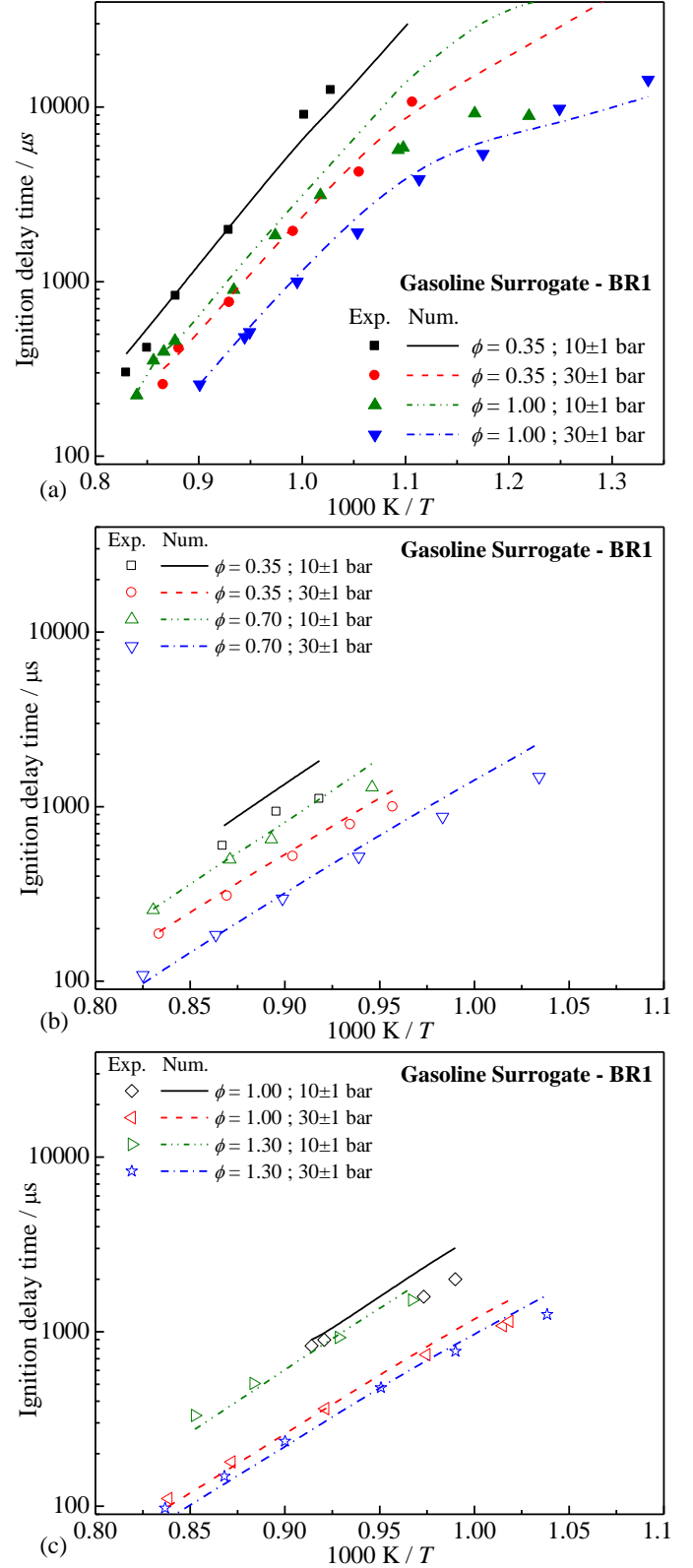
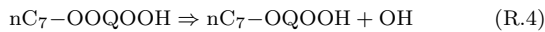
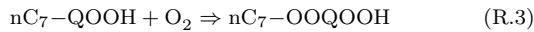
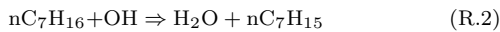
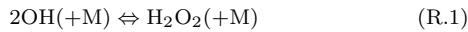


Figure 4: Experimental data (symbols) and numerical (lines) IDT prediction using the reduced model proposed in this work (a) HPST - IVG/UDE, (b) and (c) HPST - C3/NUIG

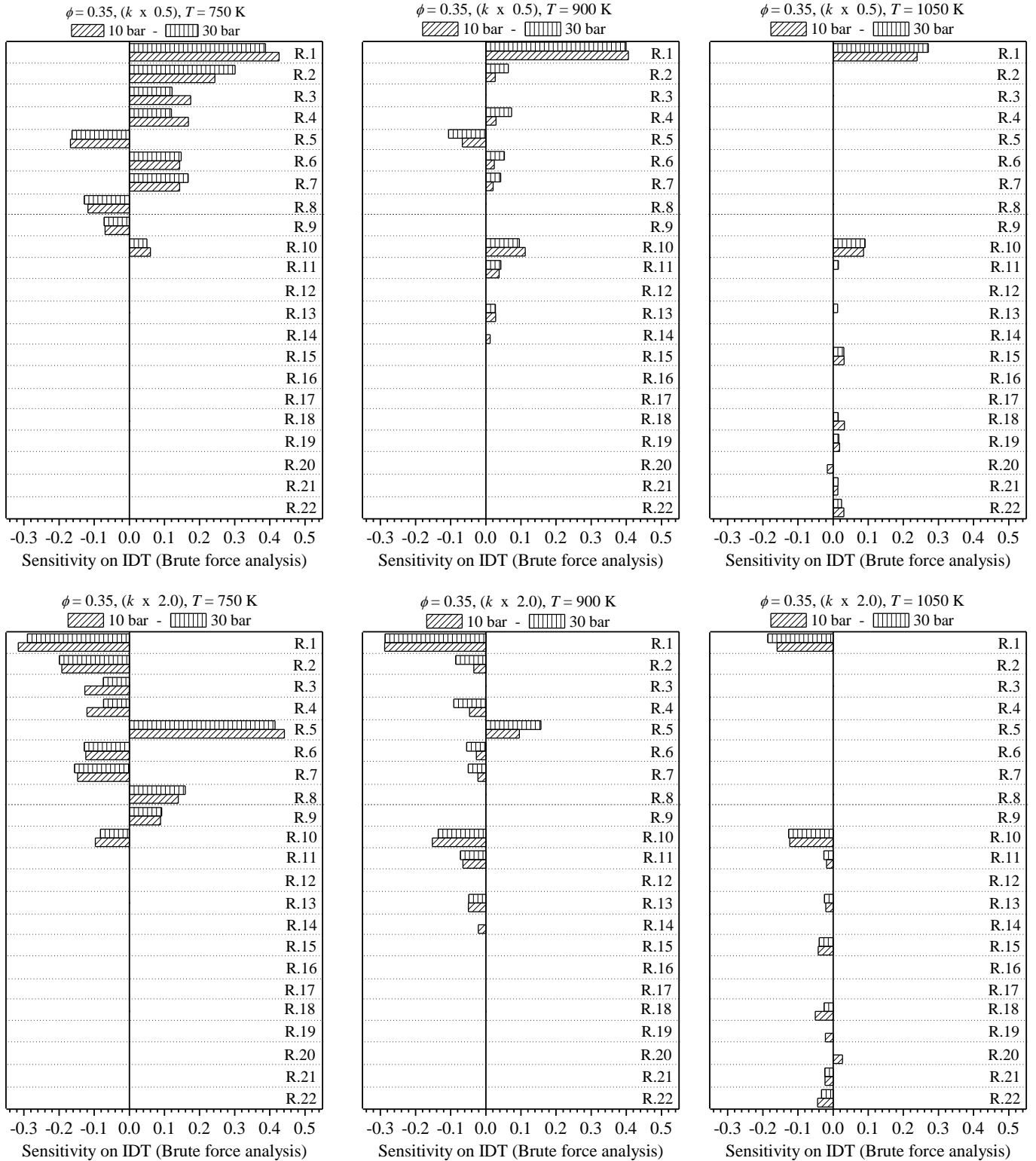


Figure 5: Brute force sensitivity on IDT for GSB1 / air mixtures at pressures of 10 and 30 bar, $\phi = 0.35$, at temperatures of 750 K, 900 K and 1050 K, and perturbation of $k \times 0.5$ and $k \times 2.0$

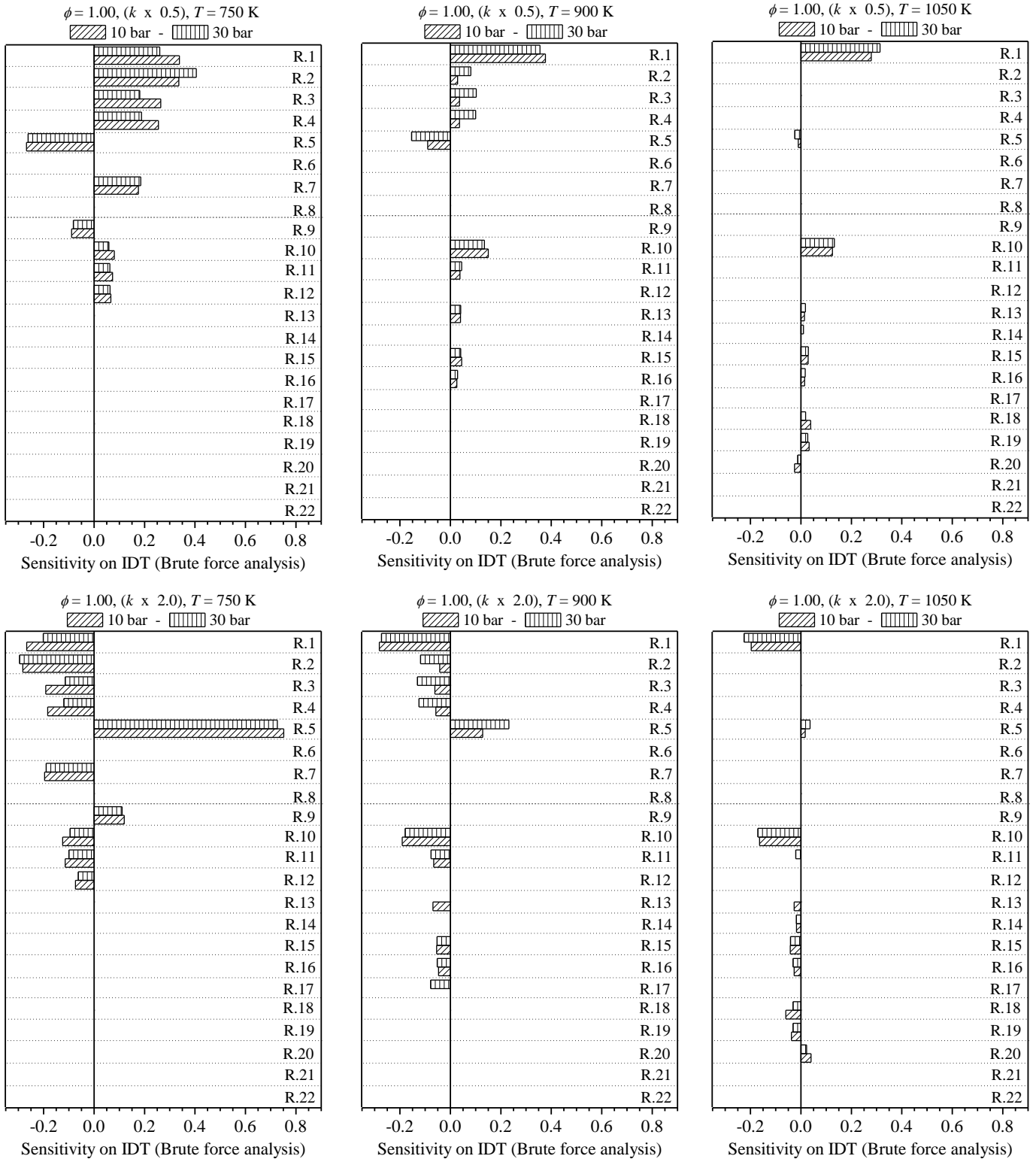
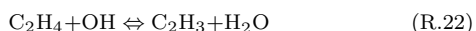
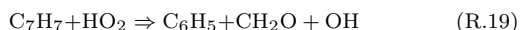
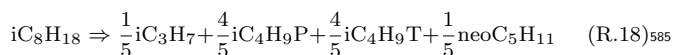
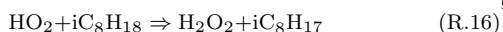
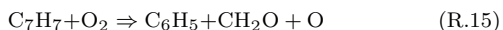
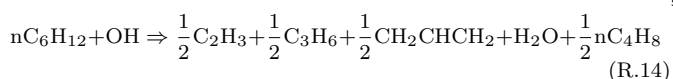
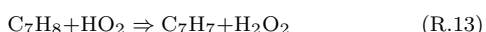
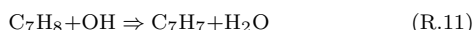
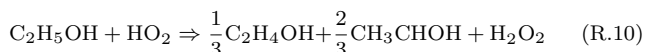
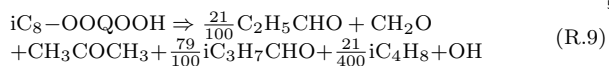
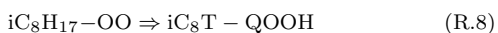
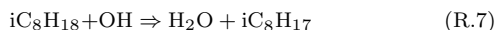


Figure 6: Brute force sensitivity on IDT for GSR1 / air mixtures at pressures of 10 and 30 bar, $\phi = 1.00$, at temperatures of 750 K, 900 K and 1050 K, and perturbation of $k \times 0.5$ and $k \times 2.0$



As expected, the predominant chain branching reaction of the H_2/O_2 system, $2OH(+M) \Leftrightarrow H_2O_2(+M)$, is important in the sensitivity analysis for all conditions, (R.1). The Arrhenius parameters of this reaction have been well defined by many research groups. At 750 K the reaction (R.5), between ethanol and $\dot{O}H$, $C_2H_5OH + \dot{O}H \Rightarrow CH_3\dot{C}HOH + H_2\dot{O}$, strongly affects the IDT, especially for $k \times 2.0$. Another important reaction with ethanol is (R.10), $C_2H_5OH + H\dot{O}_2 \Rightarrow \frac{1}{3}\dot{C}_2H_4OH + \frac{2}{3}CH_3\dot{C}HOH + H_2\dot{O}_2$, which increases IDT for $k \times 0.5$. Besides these reactions with ethanol, the addition of hydroperoxyl heptyl radicals to O_2 (R.3) and the subsequent formation of $\dot{O}H$ radicals (R.4) produced for the formation and decomposition of carbonyl hydroperoxide species are also important at low temperatures. For *iso*-octane, some internal isomerizations (R.6) increase reactivity while others (R.8) decrease it.

At 900 and 1050 K, (R.1) and (R.5) also present significant sensitivity. The other noteworthy reactions at these temperatures are those involving toluene and benzyl radical ((R.11), (R.13), (R.15), (R.19), (R.20)), mostly decreasing reactivity. For fuel-lean mixture, $\phi = 0.35$, and

1050 K, H-atom abstraction by $\dot{O}H$ from ethanol, (R.21), and ethylene, (R.22), also affected IDT predictions.

Figure 5 (lean composition) shows that reactions (R.2) to (R.9) have a relatively strong effect on IDTs at low temperatures for fuel-lean conditions. As the temperature increases the effect on IDT decreases, for 1050 K the perturbation $k \times 0.5$ has no effect on the IDT, quite the same trend can be observed for perturbation $k \times 2.0$. Reaction (R.10) shows a constant effect on IDT at low and high temperatures. From Figure 5 (stoichiometric composition) the effect of rate of perturbation $k \times 0.5$ of reactions (R.2) to (R.9) are similar to the fuel-lean condition, at high temperatures the effect on IDT is negligible, as well as for the perturbation $k \times 2.0$.

4.3. Comparison to IDT / AKI data available at literature

As mentioned in the Introduction, IDTs for several surrogates and real fuels are available in the literature. In this work published data were compared taking into account the surrogate formulation in terms of oxygenates percentage and / or the anti-knock index of the fuel / mixture of surrogates. Figure 7 shows the comparison of the measured IDT in this work to the IDT measurements from [85], [86] and [41]. All data was normalized to 30 bar and $\phi = 1.00$ using $1/p$ and $1/\phi$.

Figure 7(a) shows the strong NTC behavior of fuels FACE A, C, F and G at temperatures below 915 K. The GSBRI mixture proposed in this work does not show any NTC behavior for the experimental conditions investigated. Analyzing the composition of each fuel, the GSBRI mixture contains a low concentration of *n*-paraffins, and a high concentration of alcohol and reasonable quantities of aromatic and *iso*-paraffin, as shown in Table 1. It should be noted that FACE A, C and F fuels have low concentrations of aromatics (0.3 mol.%, 4.4 mol.% and 8.4 mol.% respectively) as well as intermediate to high concentrations of *n*-alkanes (13.2 mol.%, 28.6 mol.% and 4.8 mol.% respectively), but they have no oxygenates. These features may be responsible for the NTC behavior of these fuels. For FACE G fuel, the aromatic content (31.8 mol.%) is higher when compared to the others fuels. However, its *iso*-paraffins content is lower (38.3 mol.%), has no oxygenates and in the same way as for the FACE A, C and F fuels, these features may be the responsible for the NTC behavior of FACE G fuel. Fuels FUEL C and D, from [85], have relatively high AKI as shown in Figure 7(a), and only FUEL D includes oxygenates in the composition (8.0 mass.%). Experimental data of IDT with its related AKI information, for mixtures containing oxygenates is scarce at the literature.

Figure 7(b) shows the scaled (to 30 bar) IDT data at temperatures below those of the NTC region. It can be observed that the data can be fitted to a modified Arrhenius plot, in the form of Equation 1. Using a multiple linear regression analysis with $\ln(\tau_{30})$ as the dependent variable, $(1000/T_5)$ and $\ln(AKI)$ as independent variables identified a value of $x = -1.11$ as the AKI exponent dependency as

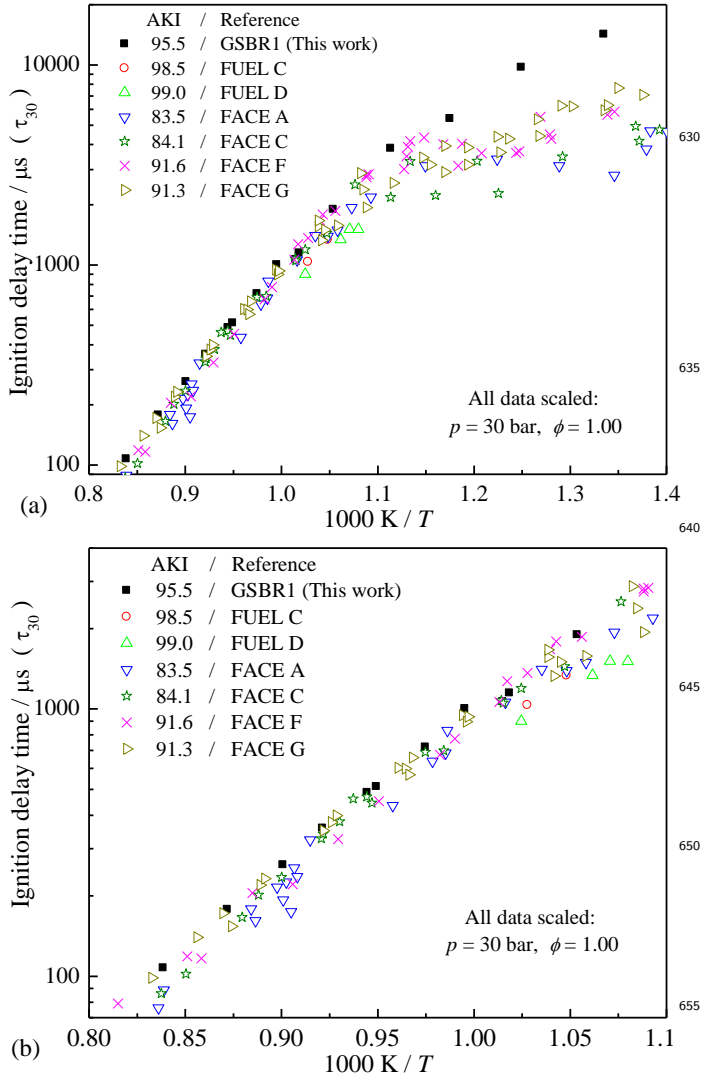


Figure 7: Scaled ignition delay times to 30 bar (τ_{30}) and stoichiometric composition ($\phi = 1.00$). References of experimental data: FUEL C and FUEL D fuels from [85], FACE A and FACE C fuels⁶⁶⁰ from [86], and FACE F and FACE G fuels from [41].

well as a global activation energy of $\approx 109 \text{ kJ/mol}$. Equation 6 shows the fitted expression in the modified Arrhenius from.⁶⁶⁵

$$\tau_{30}/\mu\text{s} = 10^{(-4.92 \pm 0.47)} \exp\left(\frac{109 \pm 1.32 \text{ kJ/mol}}{RT}\right) \times (\text{AKI})^{(1.11 \pm 0.24)} \quad (6)^{670}$$

The coefficient of determination of the multiple linear regression was $R^2 \approx 0.99$ for the experimental data shown in Figure 7(b), covering the temperature range $1225 \text{ K} \lesssim T \lesssim 915 \text{ K}$, scaled IDT to 30 bar (τ_{30}) and $\phi = 1.00$, and the anti-knock index range $95.5 \lesssim \text{AKI} \lesssim 83.5$. Because of the low number of experiments at 30 bar recorded for FUEL C and D, the six experimental points of those fuels⁶⁷⁵ were removed for the multiple linear regression of Eq. 6.

Below 915 K all the fuels holding low content of aromatics and *iso*-paraffins as well as representative quantity of *n*-paraffins shows NTC behavior, indicating that for low temperatures the IDT–AKI relationship is strong dependent on the fuel composition.

5. Conclusions

In this work, a novel, six-component, high performance gasoline surrogate (GSBR1) is proposed and investigated experimentally and numerically to determine its thermal ignition. The proposed surrogate is composed of ethanol, *n*-heptane, *i*-octane, 1-hexene, methylcyclohexane, and toluene (AL-P-I-O-N-A) with 27% of ethanol. Experiments were carried out at C3/NUIG and IVG/UDE using high pressure shock tubes with different operation characteristics (double diaphragm at C3/NUIG and single diaphragm at IVG/UDE). The data show good agreement with one another for results in the overlap temperature and pressure ranges from both shock tubes, as shown in Fig. 3(c).

A modified Arrhenius equation was developed using multiple linear regression for experiments with temperatures higher than 900 K. Pressure and equivalence ratio dependence coefficients of 0.72 and 0.62 (respectively) were obtained from the fit, as well as a global activation energy of $\approx 109 \text{ kJ/mol}$.

A simplistic approach to mechanism reduction, based on the elimination of reactions with no relevant rate of progress was used in order to reduce an extensive detailed kinetic model (hierarchically constructed with more than 17800 reactions). The reduced, though still detailed, kinetic model with 4885 elementary reactions among 326 chemical species was used for numerical simulations and its predictions were compared with the experimental data obtained herein. The reduced kinetics model reproduced relatively well the experimental results in the high temperature range, and the accuracy increases as the mixture stoichiometry increases. Moreover, the proposed reduced model reproduces the bend of the experimental data for $p = 30 \text{ bar}$ and $\phi = 1.00$ at low temperatures.

It was observed that for low temperatures the proposed reduced kinetics model agreement with data was only qualitative. In order to understand the likely cause of this discrepancy, a brute force sensitivity analysis on IDT was performed, elucidating of this form the more influencing reactions. Work is currently continuing on identifying the chemistry and surrogate species and H-atom abstraction species resulting from the decomposition of the surrogates, the brute force sensitivity analysis identifying the more important reactions controlling reactivity in the mechanism, to be considered for further analysis and optimization. For example, it was observed that reactions involving ethanol, *iso*-octane and toluene reacting with OH and HO₂ showed significant sensitivity for IDT, being noteworthy that these three surrogates species represent around 77 % of the GSBR1 composition.

The experimental data obtained in this study was compared to data available in the literature in terms of anti-knock index at a scaled pressure of 30 bar for the stoichiometric condition. A modified Arrhenius equation was then fitted and it elucidated an AKI dependence exponent of -1.11 for the data used in the multiple linear regression. This means that the higher the AKI, the longer is the IDT, independent of fuel composition (chemical groups). At temperatures below the NTC region, that trend should be confirmed with further investigations by compiling a sufficient volume of experimental data. At low temperatures all of the fuels with low concentrations of aromatics and *iso*-paraffins as well as appreciable quantities of *n*-paraffins shows NTC behavior, indicating that for low temperatures the IDT–AKI relationship strongly depends on the fuel composition.

Acknowledgments

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